PERFORMANCE OF A PYRAMID SOLAR STILL USING AIR-COOLED GLASS COVER: AN EXPERIMENTAL STUDY

M. A. Tawfk^{*}

ABSTRACT

Cooling the glass cover is considered one of the most effective modifications that affecting the performance of any solar still, particularly at summer season. Many previous studies focused on the water cooling glass cover, but it is important to study another cooling technique to avoid using potable or saline water in this process. Thus, this study aims to investigate the possibility of enhancing the performance of a passive square pyramid-shaped solar still in summer season through cooling the glass cover using controlled stream of cooled air. For this purpose, the solar still was coupled to ice-cooling unit provided with a high pressure fan in trial to reduce the temperature of the blowing ambient air over the glass cover. Solar still performance was evaluated using saline water (15000ppm) depth of 4cm without cooling as a control treatment and air-cooled glass cover under different values of air velocities and cooling tactics with taking into consideration the solar still temperatures, productivity and instantaneous efficiency. The obtained results revealed that, the increase of the cooled air velocity from 1.4 m/s (natural wind) to 5 m/s and cooling tactic of 20_{min} on -10_{min} off gave a remarkable increase in water-inner glass temperature difference (ΔT_{wei}) from 10 to 21°C and the productivity from 0.505 to 0.645 L/m^2 .h at the peak performance hour which led to achieve the highest accumulated yield of 3.545 L/m^2 .day and instantaneous efficiency of 43.2% with an increment of about 17 and 10.8%, respectively higher than solar still without cooling. Additionally, the air velocity of 7 m/s has irrelevant effect on the solar still performance, but on the contrary it gave less improvement. Hence, it is obvious that the air-cooled glass cover enhanced the solar still performance.

Keywords: *pyramid-shaped solar still, cooling, glass cover, air velocities, cooling tactics, solar still performance*

*Assistant. Prof., Agric. Eng. Dept., Fac. of Agric., Zagazig Univ., Egypt.

INTRODUCTION

he reduction of potable water sources availability and contamination resulting in a high shortage in the pure drinking water quantity all over the world and this problem will be aggravated with the rapid increase of population and the human activities against the environment. Moreover, the expensive transportation is a tough barrier to provide the communities in desert, remote and isolated regions with adequate fresh water. Solar still is considered a simple rout to produce potable water from saline water with relatively low cost in structure, operation and maintenance (Velmurugan and Srithar, 2011). Solar still can provide the mentioned regions with potable water in small scale, where the solar energy and saline water are abundantly, or if there is no other sources of energy (Tiwari et al., 2003). In the same time, the major disadvantage of solar still is the low productivity of the distilled water and can't compete with the other desalination systems (Nafey et al., 2002), noting that the maximum efficiency of the conventional solar still is being around 50% (Kaushal, 2010). So, the daily productivity of solar still is required to be enhanced continuously. The main factors affecting the productivity of solar still are the solar radiation intensity, wind speed, ambient temperature, water-glass cover temperature difference, free surface area of saline water, absorber basin area, inlet water temperature, glass cover angle, brine depth (Nafey et al., 2000; Samee et al., 2007). Furthermore, various modifications to enhance the solar still productivity and efficiency such as; using internal and external reflectors (Tanaka and Nakatake, 2006), black rubber (Nafey et al., 2001), black stones (Tawfik, 2012) and wicked evaporation surface (Kabeel, 2009). One of the most effective modifications to improve the solar still productivity is cooling the glass cover (Kalidasa et al., 2008). The rate of condensation can be improved by decreasing the temperature of glass cover the glass cover temperature can be decreased by cooling using water, air, or combination between them by using the flowing water air on the glass cover (Suneesh et al., 2014). The most of cooling process techniques were performed using hoses, but the water sprinkler (Tarawneh, 2007) also investigated. Somwanshi and Tiwari (2014) addressed the effect of water film above the glass cover of single slope still using water at

ambient temperature and the cold water introduced by the evaporative cooler. They concluded that the cold water increased the annual productivity by about 41.3 to 56.5% and the water at ambient temperature from 21.8 to 30.1.On one hand, some literatures indicated that, the cooling glass cover of different solar still designs enhances the daily productivity up to 11.82% for double slope still (Zeroual et al., 2011); 8.2% for stepped still (El-Samadony and Kabeel, 2014); 32.8% for triple solar still integrated with parabolic concentrator (Sirthar et al., 2016).On the other hand, the improper water flow rate and still design leads to diminished the incident solar radiation on the still (Omara et al., 2017) and consequently the productivity and thermal efficiency of still will be declined. This is considered as a major disadvantage of water cooling technique, in addition to wasting a portion of potable water in the cooling process that makes the still performance is not effectively. Generally, limited attempts were executed to investigate the influence of flowing air on the glass cover on the performance of solar still. Al-Garni (2012) used an external fan for cooling the glass cover of double slope solar still by the flowing air in winter season. He concluded that the external fan gave more productivity with lower depths of brine not exceed 1 cm, whereas the productivity declined by about 4 and 8% by increasing the wind speed to 7 and 9 m/s, respectively. El-Sebaii (2004) summarized that, the single effect passive solar still has a critical brine depth which beyond the distilled water productivity increases as wind velocity increases. The numerical calculations indicated that the depths below the critical depth leads to decrease the productivity by increasing the wind velocity until typical velocity (10 and 8 m/s for the summer and winter seasons, respectively). The critical depth of basin water for the investigated single effect passive stills was found to be 4.5 cm. Hence, most of previous studies are focused on simulating and numerical calculations for the effect of wind speed on the still performance. Regarding this work, there is no previous literatures about practical trials for cooling the glass cover of solar still by a controlled or regulated stream of air. As the pyramidshaped solar still has large condensation area (Taamneh and Taamneh, 2012), so this design of solar can help to maximize the distilled water productivity (Bhardwaj et al., 2015). Nayi and Modi (2017) indicated

that, the pyramid solar still doesn't require orientation or tracking mechanism, cheap, simple in structure, large condensation area, high productivity, no shadowing on the basin brine. The efficiency of this type of solar stills can reach about 50% (**Wasouf** *et al.*, **2011**). Practically, the glass cover sheets with small inclination angle that corresponding to the latitude of experimental site (30.5°) has small enclosure in addition to the small condensation area. Therefore, the present paper aims to investigate the possibility of enhancing the productivity and thermal efficiency of a passive square pyramid-shaped solar still that has relatively high glass inclination angle (up to 45°) through cooling the glass cover using controlled stream of cooled air to make difference between the inner and outer surface of the glass cover to increase the condensation rate under the Egyptian climatic conditions.

MATERIALS AND METHODS

The practical experiments were performed at Zagazig City, Egypt (*Lat.* $30^{\circ} 35^{\vee}/N$, *Long.* $31^{\circ} 31^{\vee}/E$) during September, 2017. In the present work, the performance of a square pyramid-shape solar still was using one of the most effective modifications that represents in cooling effect on glass cover by regulated cooled-air stream.

1. The experimental setup

1.1. The saline water

The saline water used in this study was brackish water (15000 ppm).

1.2. The experimental solar desalination system

The experimental solar desalination system is mainly consists of a solar still unit integrated with cooling unit, as shown in Fig.(1). The components of desalination system can be described as follows:

1.2.1. Solar still unit

The solar still unit consists of a passive square pyramid-shape solar still and the saline water tank. The still was fabricated in local workshop at Zagazig city, Egypt. The solar still has a square basin that made of galvanized iron sheet with 0.15 cm in thickness. The basin was constructed with square area of 0.64 m² (80×80 cm) and 7cm in depth which painted from inside with a synthetic black matt paint. The bottom and the side –walls of the basin were coated from outside with 10 cm of glass wool layer as heat insulator to prevent the heat leakage to ambient. The basin was contained in a square wooden box with inner dimensions of $100 \times 100 \times 17$ cm, and 0.03m in thickness.



Fig.(1): The experimental solar desalination system.



Fig.(2): Schematic diagram of the modified solar desalination system

1-Pyramid solar still, 2-Wooden box, 3-Glass wool, 4-Saline water basin, 5-Saline water, 6-Graduated bottle, 7- Air distribution hose with vents, 8- Ice, 9-high pressure fan,10- Electric motor, 11- By-pass pipe, 12-Control valves, 13- Saline water tank, 14-Cooling basin

The wooden container was putted on four poles at height of 60 cm above the ground. The solar still was covered with four triangle clear panels of commercial glass with surface area of 0. 187 m² (93.5 Base×40 Height cm)for each panel and total area 0.75 m² at inclination angle of 45° on horizontal and 0.3 cm in thickness, as shown Fig(2) the pyramid shape cover without frame was created by gathering the glass sheets using silicon rubber sealant. The pyramid glass cover was provided from inside with inclined U shaped troughs to collect the distilled water. A rubber gasket was kept between the glass cover and the wooden container to maintain the heat within the still. Two plastic bottles were connected to the trough by hoses for collecting the still productivity. A 30 L in capacity plastic tank was used to feed the still with the saline water by hose providing with controlling valve. The feeding mechanism depends on the syphonic effect due to placing the tank at 100 cm above the basin level.

1.2.2. The cooling unit

This unit includes the basin filled with ice bottles (replaced frequently), aluminum serpentine, air distribution hose as well as centrifugal fan. This system has basin made of iron sheet that painted from inside and outside anti-corrosion material with overall dimensions bv using of 42L×42W×40D cm and covered by 10 cm in thickness polystyrene panel provided with reflective film, as shown Fig.(1). An aluminum serpentine works as heat exchanger during passing the blowing air through it to transfer the heat of air to ice bottles. This serpentine has many tubes with an internal diameter of 1.200 cm and external diameter of 1.270 cm (1/2 inch). The serpentine tubes were separated by 14 cm apart to increase the length of air path as possible. The tubes were fixed on a frame at height of 20 cm from the bottom of basin. Two vertical tubes with same mentioned dimensions, the input tube which connected with air fan by flexible plastic hose and the other is the output tube that connected to a plastic Tshape joint for air distribution. Air was supplied to the serpentine and then the distribution hose by high pressure centrifugal fan (Model: SAVT, 220V) with nominal speed 3000 rpm, motor power of 0.735 kW (1hp), maximum air volume 660 m^3 /h. The fan was provided with air regulator pipe (by-pass) to control the supplied air velocity, as displayed in Fig (2). The distribution hose is made from plastic with 0.635 cm provided with

vents (0.5 cm in diameter) and placed at 10 cm apart. The distribution hose was fixed around the lower edge of glass cover using bonding material (silicon) to secure a continuous stream of air over every face of the glass cover. The hose connected to the T-shaped joint by tapered tube (1.27/0.635 cm)

2- Methods

2.1. The experimental procedures

All practical experiments were carried out during the period which started from 9 am to 5 pm. Moreover; all readings of temperatures, solar radiation intensity and the fresh water production were recorded every hour in ml. Performance of the passive pyramid solar still without cooling (control treatment) and with air cooling glass cover was studied under at saline water depth of 4cm. For the air cooling tests, the solar still was evaluated under the following variables:

- 1- Three levels of air velocity over glass cover (2.5, 5 and 7.5 m/s).
- 2- Three different exposure intervals times of 5 $_{min}$ on -10 $_{min}$ off (Tc₁), 10 $_{min}$ on-10 $_{min}$ off (Tac₂) and 20 $_{min}$ on -10 $_{min}$ off (Tac₃).

2.2. Measuring and Determinations

2.2.1. Temperature and solar radiation intensity

As displayed in Fig.(3-a), the temperatures of the ambient, supplied cooled air, saline water, inner and the outer glass cover was measured using K-type thermocouple sensors were plugged to the multi-channels digital data logging thermometer (Model: TM747 DU 4-Channel, Taiwan) with resolution of 0.1°C,.Whereas, the solar radiation intensity was measured using solarimeter (TES-132,TENMARS, Taiwan), with measuring range of 0-2000 W/m², resolution 0.1 W/m² and accuracy \pm 10 W/m². The velocity of air over the glass cover that corresponding a certain openings of the by-pass pipe valve as well as the natural wind were measured using a probe anemometer (TM-4001/4002 Hot Wire-TENMARS, Taiwan) in range of 0.01 to 25.00 m/s, resolution 0.01 m/s and accuracy \pm (3% of reading+1.6% FS), as depicted in Fig(3-b). 2.2.3.

2.2.2. The solar still productivity and instantaneous efficiency (ηi)

The passive pyramid solar still productivity was conducted by weighting the collected fresh water in the bottles every hour and consequently the accumulated productivity can be estimated.



Fig. (3) Instrumentations a) digital thermometer and solarimeter; b) measuring the air velocity over glass cover.

The instantaneous efficiency is an indicator to the amount of the exploited solar energy by the solar cooker. The instantaneous thermal efficiency (η_i) can be calculated every hour using the relation given by (**Duffie and Beckman, 1991**) as follows:

$$\eta_i = \frac{m_D h_{fg}}{AgG} \times 100 ,\%$$

Where:

 m_D = production rate of the solar still, Kg/h

 h_{fg} =water latent heat of evaporation, (2260 kJ/kg)

G = solar radiation flux, kJ/m².h

 A_g = the glass collecting area, m²

RESULT AND DISCUSSION

1- Effect of the cooled air velocity and cooling tactics on solar still temperatures

In the present study, the performance of a pyramid shaped solar still was investigated with and without air cooling glass cover under average natural wind speed of 1.4 m/s throughout the experimental period that

extended from 31/8 to 9/9/2017. The variation of the solar still temperatures including the ambient air (T_a) , saline water (T_w) , inner (T_{gi}) , outer (Tgo) surface of the glass cover and consequently the water - inner glass difference (ΔT_{wei}) as well as the solar radiation intensity (SRD) are plotted against time of day in Fig.(4).Regarding to air cooling glass cover, the outer surface of the cover subjected to regulated cooled air stream with average temperature of 28°C using different tactics involving certain exposure times and intervals of 5_{m in}on -10_{min} off (Tac₁), 10_{min}on -10_{min} off (Tac₂) and 20_{min}on -10_{min} off (Tac₃). As a general trend in all experimental days, the hourly solar radiation intensity during the forenoon hours increased rapidly till it reaches the maximum value at noon hour, then it tends to decrease gradually until the sunset hours, whereas the saline water temperature in still basin reached its peak value after the noon hour, then it takes the same trend of SRD distribution during afternoon period. The obtained results showed that, the maximum temperature of saline water decreased slightly by increasing the air velocity from 1.4 m/s (natural wind) to 5 m/s (cooled air) over the glass cover using 20_{min}on -10_{min} off as cooling tactic combined with an apparent increase for the saline water-inner glass temperature difference (ΔT_{wgi}) around noon. But further increase in cooled air velocity up to 7 and under all cooling tactics the T_w and ΔT_{wei} will be diminished. Fig.(4) illustrated that, increasing the air velocity from 1.4 to 5 m/s (cooled air) and cooling tactic of 20_{min} on -10_{min} off caused a reduction in T_w from 71 to 67°C followed by a clear increase in ΔT_{wgi} from 10 to 21°C at the performance peak hour of 1 pm.

Simultaneously, the inner and outer surfaces of glass cover temperatures are taking the same trend of the T_w . It was found that, the ΔT_{wgi} is still relatively low during the morning using the cooling tactics comparing to the still without cooling due to the heat of convection, radiation and evaporation as well as the solar radiation intensity are still low in this period, as depicted in Fig.(4). Concerning to the air velocity of 7m/s, the data showed that the T_w decreased under all tactics around noon to reach the lowest value of 63°C with a moderate values for ΔT_{wgi} and a remarkable decrease at before and after noon time.



Fig. (4): Effect of air velocity and cooling tactic on the solar still temperatures.

It is obvious that the air velocity up to 5 m/s and more exposure time and interval will lead to encourage the increase of evaporation heat flux within the still but at 7 m/s this process increased slightly particularly around noon only and this then the still thermal performance will be retarded. As results, the air velocity of 5 m/s and cooling tactic Tac₂ (20_{min} on - 10_{min} off) gave a considerable saline water temperature and the highest saline water –inner glass temperature difference.

2-Effect of the cooled air velocity and cooling tactics on productivity and accumulated yield of the solar still

The glass cover with no excessive cooling process is playing a vital role for enhancing the condensation rate and consequently the solar still productivity by offering a high temperature difference between the saline water and glass cover throughout the daylight. So, the effect of air velocity and cooling tactics on productivity and accumulated yield of the solar still is shown in Fig. (5). As general trend, the hourly distillate output of the solar still increased rapidly from zero at the beginning of the experimental day to its peak value at 1 pm, then it tends to decrease especially under the cooling process due to the reduction in the heat retention within the still, which causes also slow down the increase of accumulated yield at afternoon period. Regarding the highest hourly productivity, data showed that the increase of air velocity from 1.4 m/s to 3 and 5 m/s (cooled air) at cooling tactic of 20_{min} on -10_{min} off as cooling tactic the highest hourly distillate at noon increased from 0.505 to 0595 and 0.645 L/m².h with an increment of about 15.12 and 21.7%, respectively, while this value was 0.615 L/m².h at air velocity of 7m/s under the same tactic. It is clear that the increase of cooled air velocity up to 7 m/s gave a close or may be lower values of productivity around noon only but remarkable decrease in other periods of day which may reduce the accumulated yield under all cooling tactics comparing to lower air velocities. It is obvious that the effect of cooling process to enhance the productivity was ceased at air velocity of 7 m/s and it becomes irrelevant. As an explanation, saline water has a high heat capacity comparing to the glass cover, but the high cooled air velocity with more exposing time will slightly reduce the saline water temperature and glass.



Fig.(5):Effect of air velocity and cooling tactic on the solar still productivity and accumulated yield

With regard to the best accumulated yield, the increase of air velocity from 1.4 m/s (without cooling) to 5 m/s (cooled air) would increase the accumulated yield from 2.905 to 3.247, 3.332 and 3.501 L/m².day at cooling tactics of 5_{min} on -10_{min} off , 10_{min} on -10_{min} off and 20_{min} on -10_{min} off, respectively. Nevertheless, the accumulated yield was decreased by increasing the velocity up to 7 m/s to 3.21, 3.29 and 3.490 L/m².day at the same tactic respectively, as displayed in Fig.(5).The obtained results indicated that the highest accumulated yield of 3.545 L/m^2 .day was achieved using the cooled air velocity of 5 m/s and cooling tactic 20_{min} on -10_{min} off (Tac₃) with an increment of about 17% higher than solar still without cooling, whereas the air velocity of 7 m/s did not improve the solar still productivity.

3- Effect of air velocity and cooling tactics on the solar still instantaneous efficiency (ηi)

Since the solar still instantaneous efficiency mainly depends on the hourly distillate output, solar radiation intensity and glass condensation area, hence preventing of the heat losses from glass to ambient air by the glass cover cooling will definitely increase the condensation rate which is play an important role for increasing the distillate output and subsequently the solar still thermal instantaneous efficiency will improve. Effect of air velocity and cooling tactics on the solar still instantaneous efficiency is illustrated graphically in Fig. (6).



Fig.(6):Effect of cooled air velocity and cooling tactic on the solar still instantaneous thermal efficiency.

For the highest values of efficiency at noon, the increase of air velocity from 1.4 m/s (without cooling) to 5 m/s (cooled air) increased the instantaneous efficiency from 32.4 to 36.6, 38.47 and 43.2% at cooling tactic of 5_{min} on -10_{min} off , 10_{min} on -10_{min} off and 20_{min} on -10_{min} off, respectively. This may be due to the increase occurred in saline waterinner glass difference without notable change for the heat stored in the water bulk. By increasing the cooled air velocity to 7 m/s, the solar still instantaneous efficiency decreased and the value become closed to the lower velocities under all cooling tactics. According to the previous discussion, the increase of cooled air velocity up to 5 m/s raised the solar still instantaneous efficiency by about 10.80% higher than solar still without cooling, while air velocity of 7 m/s gave a less enhancement.

CONCLUSION

In the present work, the cooling effect on the temperatures, productivity and instantaneous thermal efficiency of a conventional passive pyramid solar still was investigated by using a controlled and regulated cooled-air stream over the glass cover. The solar still was coupled to iced-cooling unit to reduce the temperature of the supplied air by the fan. According to the obtained results, the increase of air velocity from 1.4 m/s (natural wind) to 5 m/s (cooled air) and cooling tactic of 20minon -10min off accompanied by slight decrease in the saline water temperature followed by a remarkable increase in water-inner glass temperature difference (ΔT_{wgi}) from 10 to 21°C and the productivity from 0.505 to 0.645 L/m².h. The highest accumulated yield of 3.545 L/m².day and instantaneous efficiency of 43.2% were achieved at air velocity of 5 m/s and cooling tactic of 20_{min}on -10_{min} off with an increment of about 17 and 10.8%, respectively higher than the still without cooling. Also, the air velocity of 7 m/s has irrelevant effect on the solar still performance. Ultimately, it can use the PV system in future to operate the electric motor in order to make the system more economic.

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<u>الملخص العربى</u> أداء المقطر الشمسي الهرمي بإستخدام الغطاء الزجاجي المبرد بالهواء: دراسة تجريبية محمد على توفيق*

تبريد الغطاء الزجاجي يعتبر من أهم التعديلات المؤثرة علي الإنتاجية من الماء المقطر و الكفاءة الحرارية لأي مقطر شمسي و خاصة في فصل الصيف. يوجد العديد من الدراسات السابقة التي تتناول تبريد الغطاء الزجاجي بإستخدام الماء لتحسين أداء المقطر و لكن من المهم إستخدام طريقة أخري للتبريد بدون إستخدام ماء الشرب أو حتي الماء المالح. لذلك فإن هذة الدراسة تهدف إلي بحث إمكانية رفع معدل الأداء للمقطر الشمسي الهرمي ذو القاعدة المربعة الغير فعال من خلال إستخدام تبار من الهواء الجوي المبرد و المنظم لتبريد سطح الزجاج في فصل الصيف. ولتحقيق هذا الغرض فإنه تم توصيل المقطر الشمسي بوحدة تبريد الهواء بالثلج في محاولة لتخفيض درجة حرارة الهواء الجوي المدوع في النظم بواسطة مروحة عالية في محاولة لتخفيض درجة حرارة الهواء الجوي المدفوع في النظم بواسطة مروحة عالية تركيز الأملاح ١٥٠٠٠ جزء في المليون) وذلك بدون تبريد للغطاء الزجاجي كمعاملة مرجعية ، وبإستخدام الهواء المبرد تحت قيم مختلفة لكل من سرعة الهواء البرحاض مع المياء الأحذ م وباستخدام الهواء المبرد تحت قيم مختلفة لكل من سرعة الوجام التوصي ، واسق تركيز الأملاح ١٥٠٠ المقطر الشمسي الغير فعال باستخدام عمق للمياه المالحة مقداره ٤ سم) وباستخدام الهواء المبرد تحت قيم مختلفة لكل من سرعة الهواء الزجاجي ونسق تأثير تلك المتغربات علي درجات الحرارة الماصل بين فترات التعرض) مع الأخذ في الأعتبار وباستخدام الهواء المبرد تحت قيم مختلفة لكل من سرعة المواء المبرد علي الزجاج ، ونسق تأثير تلك المتغيرات علي درجات الحرارة المقطر الشمسي والإنتاجية والكفاءة اللحظية. فقد تأثير تلك المتغيرات علي درجات الحرارة للمقطر الشمسي والإنتاجية والكفاءة الحظية. فقد أوضحت النتائج المتحصل عليها أن زيادة سرعة الهواء المبرد من ٤ م/ث (متوسـط

^{*} أستاذ الهندسة الزراعية المساعد – كلية الزراعة - جامعة الزقازيق – مصر.

الرياح الطبيعة أثناء التجارب) إلى ٥ م/ث من الهواء المبرد و نسق التبريد ٢٠دقيقة تشغيل-٢٠دقائق إيقاف قد أعطي زيادة ملحوظة لفرق درجات الحرارة بين الزجاج الداخلي و الماء المالح داخل المقطر من ١٠ إلي ٢٠ درجة مئوية وإنتاجية من ٥٠٠, إلي ٦٤٥, لتر/م٢. ساعة و ذللك في فترة أقصي تشغيل (فترة الظهيرة) و التي أدت إلي تحقيق أعلي قيمة الإنتاجية اليومية وهي ٥٤٥,٣ لتر/م٢ يوم وكفاءة لحظية ٢٠,٣٤% بزيادة تصل إلي ١٧% و ٢٠،١٠ % علي الترتيب أعلي من المقطر الغير مبرد. علاوة علي ذلك فإن سرعة الهواء المبرد ٧ م/ث كانت غير مؤثرة علي أداء المقطر بل علي العكس فقد ادي إلي إنخفاض أدائه. ومن هنا نجد ان تبريد الغطاء الزجاجي بالهواء المبرد أدي إلي تحسين اداء المقطر الشمسي الهرمي الغير فعال.